

the early reports in 1756 by William Cullen was conducted an experiment for the first time in his university [1]–[3]. Later it was developed by the Michael Faraday in 1820 by using liquefied ammonia and other gases by using high pressure and low temperatures [1]–[3]. Later in 1834 Jacob Perkins who claimed patent for the Vapor Compression Refrigeration System [1]–[3]. Researches had developed its thermophysical properties such as specific heat, density, thermal conductivity and specific heat. Hence it is evident from the open literature survey, a mixed refrigerants such as Propane /ISO-butane (R290/R600a) attracts much attention in Freezer cycle [4]. In general, combination of both carbon and hydrogen are known as hydrocarbons such as Propane and ISO-butane are hydrocarbon refrigerants are used to avoid Chlorofluorocarbons (CFCs) in the process of ozone depletion is accepted widely in the universe [5]. The usage of both combined Hydrocarbons (HCs) such as propane and ISO-butane combination which shows major advantages such as high miscibility with mineral or synthetic oil, non-toxicity, etc. [6]. Around 180 years of refrigerant history maybe around 50 substances had more or less widely used for the research. Due to sustainable reasons with varying conditions of applications for the future trends and applications a few number of natural substance such as ammonia (NH₃), hydrocarbons (HCs) and carbon dioxide (CO₂), helium (He), hydrogen (H₂), water (H₂O) are used for the industrial applications and most of them are discarded due to various reasons [7]. In a refrigerant mixture propane and ISO-butane (R290 and R600a) zeotropic mixture is used in the tube supply of less liquid volatile component the saturation temperature is decreased due to the reason pressure is compensated [8]. Mixed refrigerants are highly precious due to its a combination of two different refrigerants at different composition thermophysical properties classified pure refrigerants and refrigerants mixture blends which are further reclassified based upon the property of fluids [9]. In composed classified pure refrigerants and refrigerants mixture blends which are further reclassified based upon the property of fluids [9]. In the present work, due to a research gap has analyzed that many researchers conducted different experimental results and simulation analysis to calculate thermophysical properties such as specific heat, viscosity, density and thermal conductivity. In present context, a refrigerant mixture such as zeotropic mixture combination both hydrocarbons (HCs) propane (R290) and ISO-butane (R600a) are chosen for the analysis at pressure of 3 MPa to a pressure of 7 MPa and the temperature is varying from 300–350 K in a Vapor compression refrigeration system (VCRS) and properties of refrigerant mixture for the present work is available from research Methodology (see Table 1). The molecular weight of refrigerant mixture is taken as 10 gms and refrigerant mixture is in the mass ratio of 10%–90%, 20–80%, 30–70%, 40–60% are considered density and viscosity varying with respect to temperatures plotted. Figure 1 represents schematic diagram for an industrial refrigeration system. It mainly consists of four major components such as a compressor, condenser, expansion valve and evaporator. In the compressor the vapor from low pressure gas adiabatically compressed to high pressure gas this process is also known as 'Win' process [10]–[12]. Condenser is the process which condenses the liquid from high pressure gas to high pressure liquid in this process the phase change takes place and heat is losses outside the system (Q_{out}) it is also refer to the latent heat of vaporization [13]–[15]. Expansion valve is the process where narrow passage of liquid from high pressure gas is converted to pressure liquid and vapor will be released. In the expansion valve, neither heat nor work added or rejected from the system in this process is enthalpic process (h₁=h₂) which deals with the property of the system [13]–[15]. The final stage of the vapor compression refrigeration system is (VCRS) evaporator in which low pressure liquid and vapor gas

converted to low pressure gas where the heat is added to the system (Q_{in}). In the evaporator phase change process occurs similar to condenser it is also latent heat of vaporization [11], [13], [15].

2. Materials and Methods

Yan et al [4] investigated with zeotropic refrigerant mixtures such as R290 and R600a for domestic freezer in an internal autocascade refrigeration cycle (IARC) performance of these IARC a mathematical model is used to develop the performance. The results are discussed about the pressure ratio of compressor, COP performance volumetric compressor. Richardson et al [5] investigated the performance of hydrogen and carbon in a vapor compression refrigeration system results are calculated propane and ISO-butane can be used for the better purpose under some operating conditions. Yan et al [6] study reports using zeotropic mixtures such as R290 and R600a for the modified ejector expansion cycle in this conventional ejector expansion cycle and throttling cycle is carried out. Results are presented that refrigerant effect of COP, volumetric efficiency etc. Lorentzen [7] natural substances such as ammonia (NH_3), propane (R290) and carbon dioxide (CO_2) are used as conventional fluids these fluids present shall carbon is an important factor. The ideal refrigeration or heat pump cycle for a given purpose is defined by the boundary conditions of the application and is completely independent of the refrigerants are used to enhance the thermodynamic and heat transfer properties. Mohanraj et al [8] performed an experimental work, with single evaporator domestic refrigerator using hydrocarbon mixture which means a mixed refrigerant of propane (R290) and ISO-butane (R600a) it presents that hydrocarbons have lower consumption of energy. However, it leads to high value of coefficient of performance (COP). Ardhapu et al [9] in the present investigation to calculate the overall heat transfer coefficients along with the length of heat exchangers for various mixtures has been determined for these experimental data and empirical correlations have been determined. Dalkilic et al [16] in this study experimental results of pressure drop condensation was determined by choosing two refrigerants such as R600a 1 m long horizontal and smooth with inner diameter 4 mm and outer diameter 6 mm and R134a in a vertical 0.5 m smooth copper tube with inner diameter 8.1 mm and outer diameter 9.52 mm.

3. Results and Discussion

3.1. Pressure effect on density with respect to temperature of a refrigerant mixture at different compositions.

In the present results, from Figure 1 to Figure 4 shown in below that the effect of variation in pressure at different composition varies 10%-90%, 20%-80%, 30%-70%, and 40%-60% as discussed earlier density of refrigerant mixture refrigerant increases with an increase in temperature. Figure 1 reveals that density as a function of temperature at a composition of 10%-90% of a mixed refrigerant R290 and R600a. Moreover, as the increase in temperature density of a mixed refrigerant is also increases.

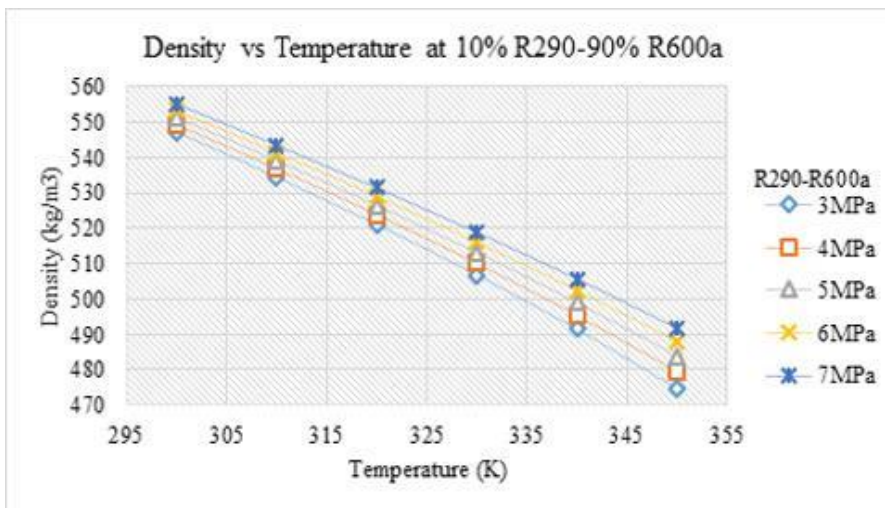


Figure1. Density vs temperature at different compositions

Figure 2 represents that density as a function of temperature at a composition of 20%-80% of a mixed refrigerant R290 and R600a. Moreover, as the increase in temperature, density of a mixed refrigerant is also increases.

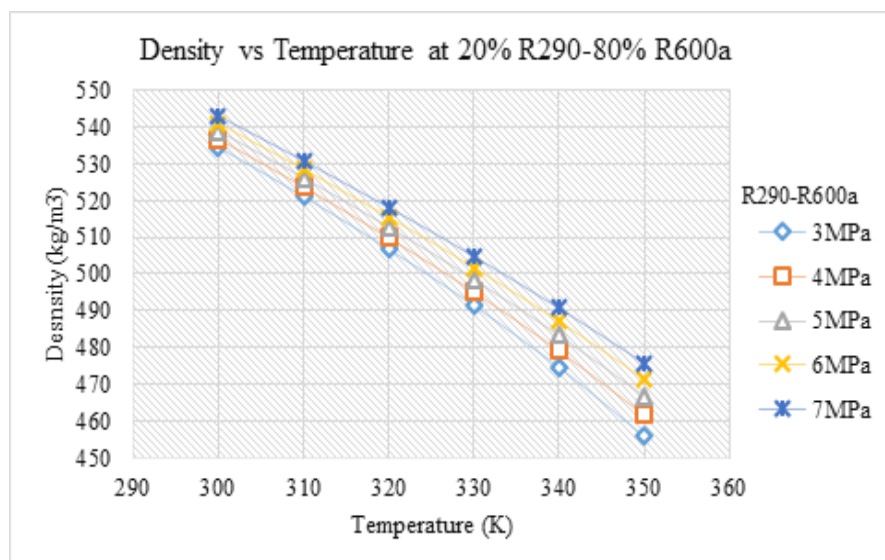


Figure2. Density vs temperature at different compositions

Figure 3 shows the variation of density with respect to temperature at a composition of 30%-70% of a mixed refrigerant R290 and R600a. Moreover, as the increase in temperature, density of a mixed refrigerant is also increases.

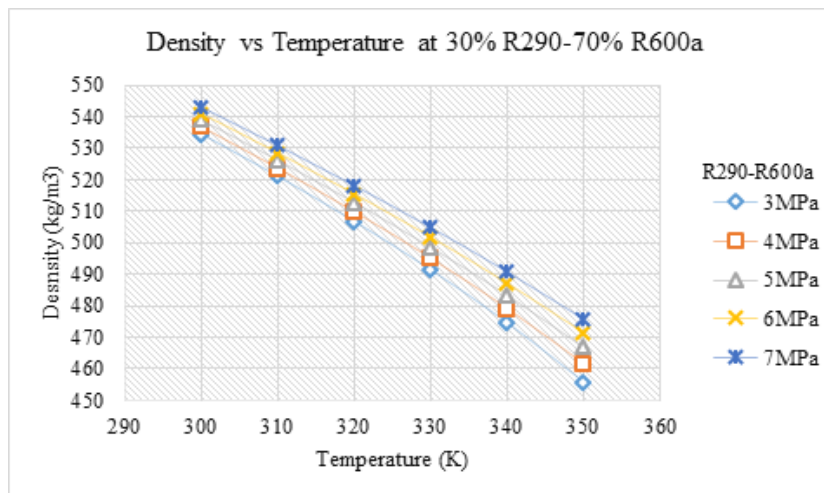


Figure3. Density vstemperatureat different compositions

Figure4showsthevariationofdensitywithrespecttotemperatureatacomposition of40%-60%ofamixedrefrigerantR290 andR600a. Moreover, astheincreaseintemperature, densityofa mixedrefrigerantisalsoincreases.

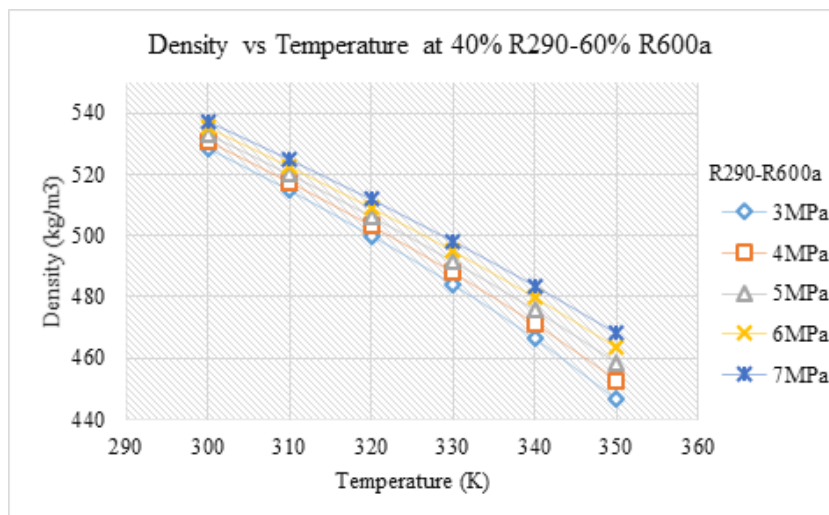


Figure 1. Density vstemperatureat different compositions

3.2. Effect of pressure on viscosity with respect to temperature of a refrigerant mixture at different compositions

In this results from Figure 5 to Figure 8 shown in below that the effect of variation in pressure at different composition varies 10%-90%, 20%-80%, 30%-70%, and 40%-60% as discussed earlier viscosity of refrigerant mixture refrigerant increases with an increase in temperature.

Figure 5 shows the variation of viscosity with respect to temperature at a composition of 10%-90% of a mixed refrigerant R290 and R600a. Moreover, as the increase in temperature density of a mixed refrigerant is also increases.

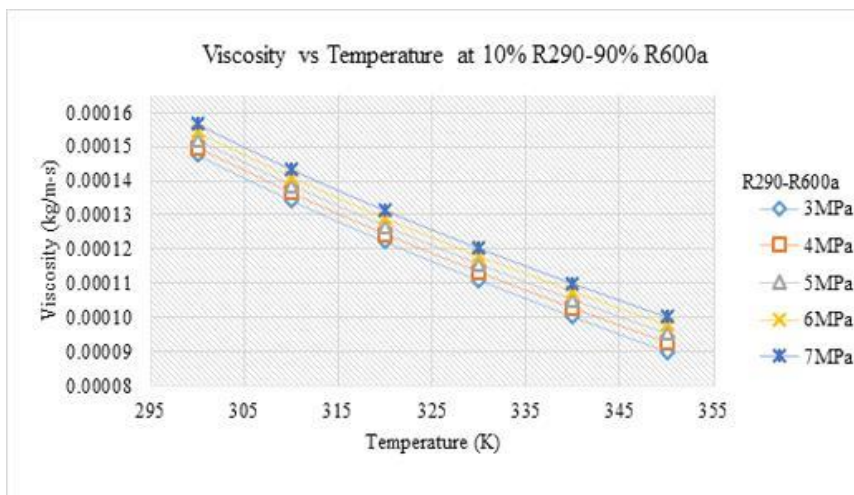


Figure 2. Viscosity vs temperature at different compositions

Figure 6 represents that viscosity as a function of temperature at a composition of 20%-80% of a mixed refrigerant R290 and R600a. Moreover, as the increase in temperature density of a mixed refrigerant is also increases.

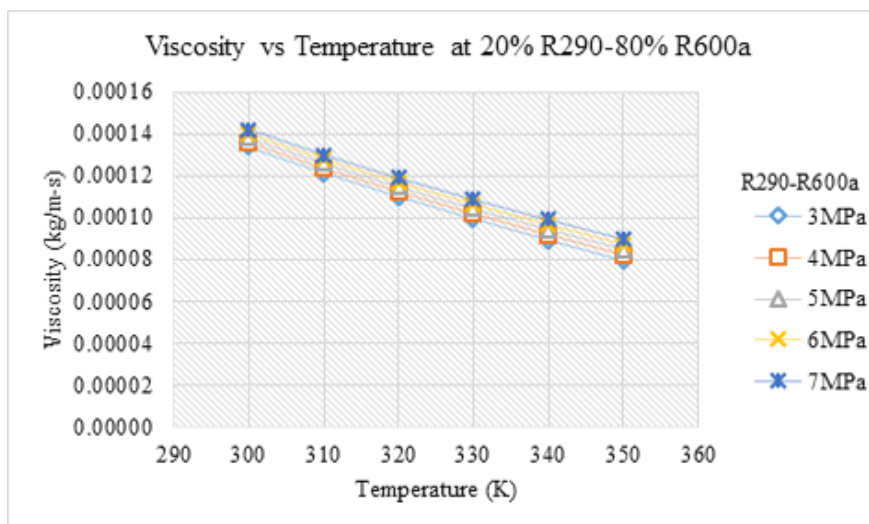


Figure 6 viscosity vs temperature at different compositions

Figure 7 shows the variation of viscosity with respect to temperature at a composition of 30%-70% of a mixed refrigerant R290 and R600a. Moreover, as the increase in temperature density of a mixed refrigerant is also increases.

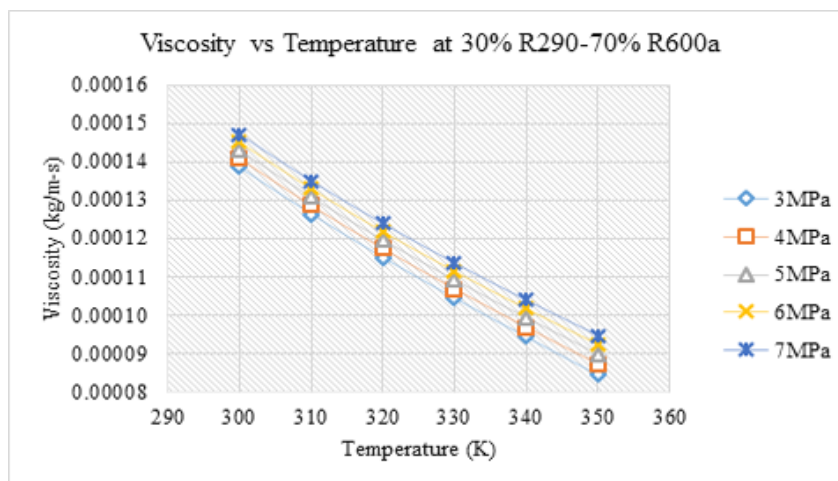


Figure7. viscosity vstemperatureat different compositions

Figure8represents thatviscosityas afunctionoftemperatureata compositionof20%-80%ofamixedrefrigerantR290and R600a.Moreover,astheincreaseintemperaturedensityofa mixedrefrigerantisalsoincreases.

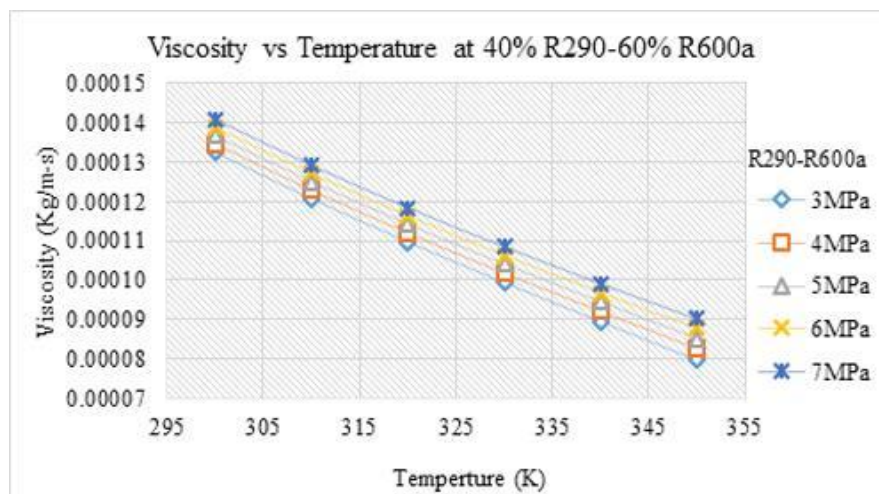


Figure8. viscosity vstemperatureat different compositions

4. Conclusion

Inthepresentresearchwork,investigationonpressureeffectatdifferentmixturerefrigerantsatdiffere ntcompositioniscarried.

Itwasconcludedthatatastheincreaseindensityandviscosityareincreaseswithincreaseintempera tureof(300-350K).

ThoughR-290(Propane)andR-600a(ISO-butane) arehighlyflammablegases,zeroozonedepletionpotentialandlessglobal warmingpotential.Itwasalsonoted

that7MPabothdensityandviscosityincreasedby4.15%and12.63%respectivelywhiletemperature waskept constant at 350K.

References

- [1] M.Duminil, "ABrief HistoryofRefrigeration,"*Int. Inst. Reprigeration*, pp.1–5,2010.
- [2] R. Cycles,C.P. Equipment,H. Rejection,and C. P.Design, "CoolingProductionEquipment and."
- [3] A.Conditioning,"AlternativeRefrigerantsand Cycles for Compression Refrigeration Systems,"2005.
- [4] G.Yan,T.Bai,andJ.Yu,"Thermodynamicanalysisonamodifiedejctorexansionrefrigerationcyclewith zeotropicmixture(R290/R600a) for freezers,"*Energy*,vol. 95, pp. 144–154, 2016.

- [5] R.N.Richardson and J.S.Butterworth, "Vapour-Compression Refrigeration System PROPa," no. July 1993, 1994.
- [6] G.Yan, H.Hu, and J.Yu, "Performance evaluation on an internal auto-cascade refrigeration cycle with mixture refrigerant R290/R600a," *Appl. Therm. Eng.*, vol. 75, pp. 994–1000, 2015.
- [7] G.Lorentzen, "The use of natural refrigerants: a complete solution to the CFC/HCFC predicament," *Int. J. Refrig.*, vol. 18, no. 3, pp. 190–197, 1995.
- [8] M.Mohanraj, S.Jayaraj, C.Muraleedharan, and P.Chandrasekar, "Experimental investigation of R290/R600a mixture as an alternative to R134a in a domestic refrigerator," *Int. J. Therm. Sci.*, vol. 48, no. 5, pp. 1036–1042, 2009.
- [9] P.M.Ardhapurkar, A.Sridharan, and M.D.Atrey, "Performance evaluation of heat exchanger for mixed refrigerant J-T cryocooler," *Cryogenics (Guildf.)*, vol. 63, pp. 49–56, 2014.
- [10] "Contents : Lesson," 2008.
- [11] M. Holt, "Air-conditioning and refrigeration equipment," *EC MElectr. Constr. Maint.*, vol. 112, no. 8, 2013.
- [12] "No Title."
- [13] C. Guide, *Air conditioning and refrigeration*, vol. 266, no. 2. 1958.
- [14] S.K. Wang, *Handbook of Air Conditioning and Refrigeration*. 2000..
- [15] H. Uchida, "Refrigeration and Air-Conditioning," *Trans. Japan Soc. Mech. Eng.*, vol. 25, pp. 913–915, 1959.
- [16] A.S.Dalkilic, O.Agra, I.Teke, and S.Wongwises, "Comparison of frictional pressure drop models during annular flow condensation of R600a in a horizontal tube at low mass flux and of R134a in a vertical tube at high mass flux," *Int. J. Heat Mass Transf.*, vol. 53, no. 9–10, pp. 2052–2064