

Effect of Pressure on Thermo Physical Properties of Mixed Refrigerant R-290 and R-600a for High Capacity Vapour Compression Refrigeration System (VCRS)

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Abstract

The concept of mixed refrigerant fluid has emerged during the past few decades from 16th century thermo physical properties as compared to base fluids. as coolants in heat transfer equipments such as heat exchangers, electronic cooling system and radiators. In the present investigation, analyze physical properties, various parameters by considering 10gms of mixed refrigerant of butane at different compositions. Results are presented for simulations carried out at a temperature range of 350K and pressure. is concluded from the result that as the temperature increases, specific heat refrigerant decreases. Similarly, thermal conductivity increases with an increase in temperature at different refrigerant. Further, as the pressure is varied from 3MPa to 7MPa while keeping the temperature at 350K, the specific heat decrease by 5.2% as well as thermal conductivity follows the opposite trend, increased by 6.9%.

Keywords:

Refrigerants, Thermophysical, Base fluids, heat transfer, Coolants, Heat exchangers.

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1. Introduction

In present scenario studies on mixed refrigerant has become versatile all over the universe, so for these reasons vapor compression refrigeration systems (VCRS) are used for cooling purposes. In general, Figure 1 represents VCRS cycle consists of four major parts such as compressor, condenser, expansion valve and evaporator. The compressor is the process where the low temperature and low pressure gaseous refrigerant is compressed isentropically to obtain high pressure super-heated

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vapor region this process is also predominately known as 'Win' process. From process 1-2 Figure 1, Figure 2, Figure 3 represents the work given by the compressor [1]–[3]. From the process 2-3 condenser process takes place in condenser the high pressure and high temperature superheated vapor is converted to high pressure and high temperature liquid refrigerant this process takes at constant pressure ($P=C$) and within the dome there will be occurrence of constant temperature process ($T=C$). In this process heat rejection will take place 'Q out' in the Figure 1, Figure 2, and Figure 3 represents process 2-3 [4]–[6]. Expansion valve is the process takes place at takes place from 3-4 in this neither heating input nor rejection of heat occur neither supply of work nor rejection of work takes it is the process enthalpy is the process where narrow cut junction will occur to supply the liquid from high pressure and temperature liquid to low pressure and temperature liquid and vapor region [7]–[9] Figure 1, Figure 2, Figure 3 represents process 3-4. Evaporator is the process where the object gets cooled this process generally takes place from 3-4 is the process represents in Figure 1, Figure 2, Figure 3 where low pressure and low temperature liquid and vapor refrigerant is converted to Vapor refrigerant. This process is also widely known as heat supply process (Q_{in}) [5], [6], and [8].

2. Materials and Methods

Gow [10]. Investigated with the elementary materials of cryogenics and 39 pure refrigerants are used to design the vapor pressure vs temperature relationship by using different type of hydrocarbon refrigerants and the cryogenic compounds the equation has developed. Richardson *et al* [11] conducted experimentally without passage of air the performance of refrigerants and concluded that propane and ISO-butane give the better performance of Coefficient of performance (COP). Lorentzen [12]. Considered thermodynamic and heat transfer properties as an important factor. Natural substances such as propane, ammonia and carbon dioxide are used as halocarbons. Scalabar *et al* in this work, pure fluids and mixtures are predicted fluid families such as alkanes and halogenated alkanes with high accuracy of dedicated equations of state (DEOS) have been proposed thermodynamically. Latra Boumaraf *et al* [13] have been proposed simulation results for the performance and characteristics of the operating cycle of refrigeration system. This simulation results include correlation of the ejector and the conservation of 1-D model. Dalkilic *et al* [14] in this study experimental results of pressure drop condensation were determined by choosing two refrigerant such as R600a 1 m long horizontal and smooth with inner diameter 4 mm and outer diameter 6 mm and R134 in a vertical 0.5 m smooth copper tube with inner diameter 8.1 mm and outer diameter 9.52 mm. Mohanraj *et al* [15] performed an experimental work, with single evaporator domestic refrigerator using hydrocarbon mixture which means mixed refrigerant of propane (R290) and ISO-butane (R600a) it presents that hydrocarbons have lower consumption of energy. However, it leads to high value of coefficient of performance (COP). Ardhapukar *et al* [16]. In the present investigation to calculate the overall heat transfer coefficients along with the length of heat exchangers for various mixtures has been determined for these experimental data and empirical correlations have been determined. Yan *et al* [17]. Investigated with zeotropic refrigerant mixtures such as R290 and R600a for domestic freezer in an internal auto cascade refrigeration cycle (IARC) performance of these IARCa mathematical model is used to develop the performance. The results are discussed about the pressure ratio of compressor, COP performance volumetric compressor. Yan *et al* [18]. Study reports using zeotropic mixtures such as R290 and R600a for the modified ejector expansion cycle in this conventional ejector expansion cycle and throttling cycle carried out. Results are

presented that refrigerant effect of COP, volumetric efficiency etc. Chen [19]. To enhance the overall system performance an internal sub-cooler with additional bypass is used. In this study modified vapor compression refrigeration cycle (MVRC) using zeotropic mixtures with addition of hydrocarbon refrigerants such as propane (R290) and ISO-butane (R600a) is used.

3. Results and Discussion

3.1. Pressure effect on specific with respect to temperature of refrigerant mixture at different compositions such as 10%-90%, 20%-80%, 30%-70%, and 40%-60% for propane (R290) and ISO-butane (R600a)

To evaluate the thermo physical properties refrigerant mixtures such as specific and thermal conductivity are evaluated for the propane and ISO-butane (R290 and R600a) are considered. Refrigerant mixture operates at a pressure of 3 MPa to 7 MPa and temperature of 300-350 K. Specific heat and thermal conductivity of the refrigerant mixture is evaluated from Figure 1 to Figure 4

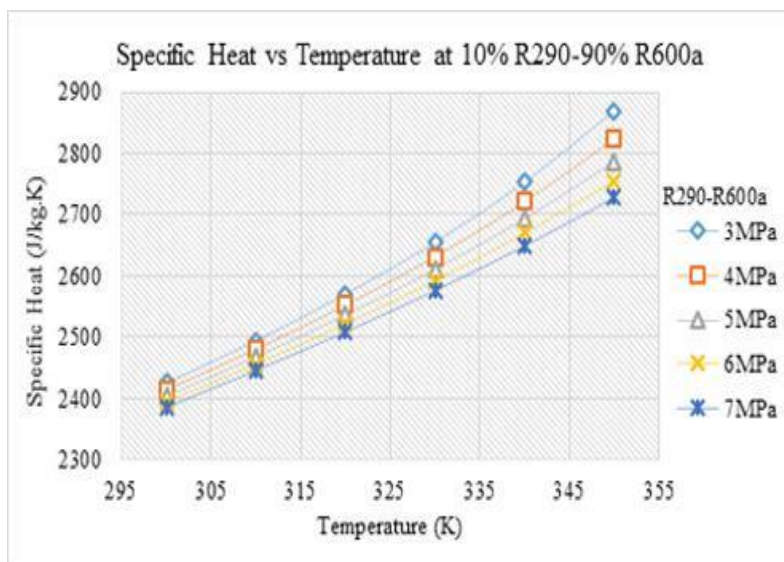


Figure 1. Specific heat vs. temperature at different compositions

Figure 1 reveals that variation of specific heat as a function of temperature at a composition of 10%-90% of a mixed refrigerant R290 and R600a. Moreover, as the increase in temperature, the effect of pressure on specific heat of a mixed refrigerant is decreasing.

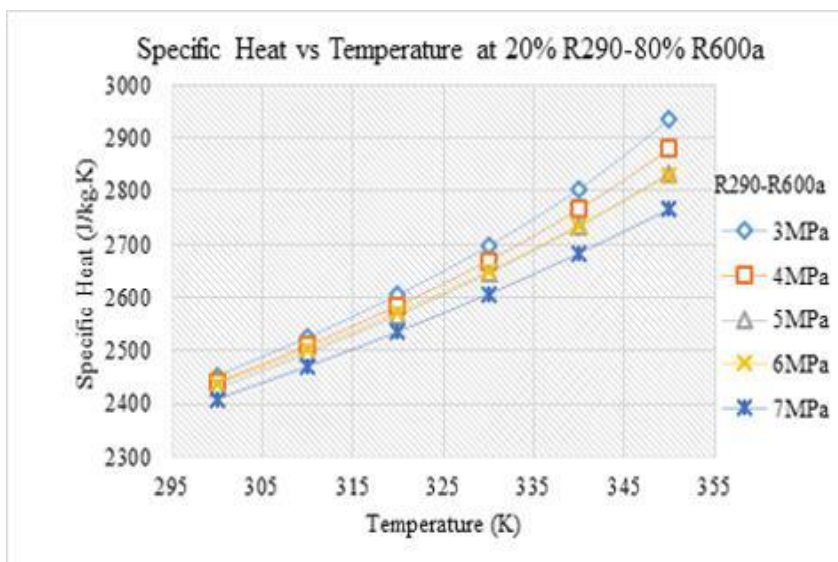


Figure2.specificheatvs.temperatureatdifferent compositions

Figure2showsthevariationofspecificheatwith respecttotemperatureatacompositionof 20%-80%ofamixed refrigerantR290and R600a.Moreover,astheincreaseintemperature,effectofpressure onspecificheatofamixed refrigerantis decreases.

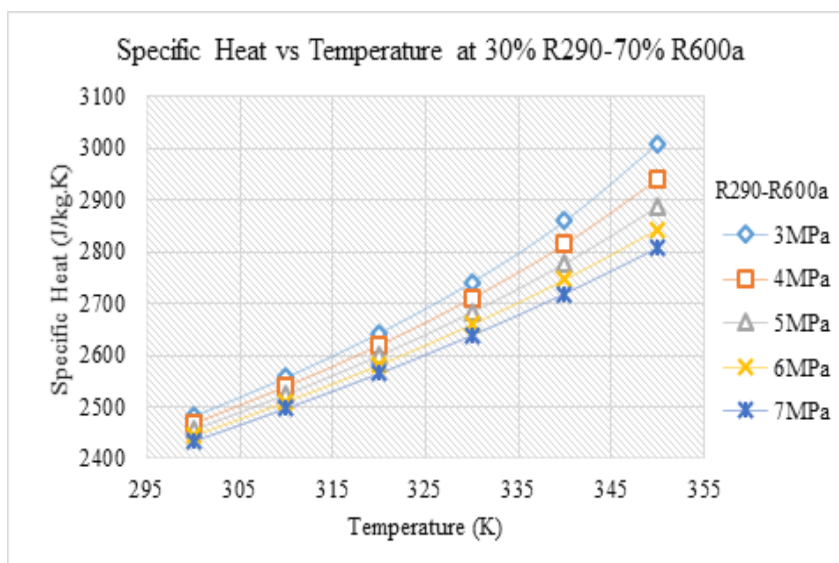


Figure3.specificheatvs.temperatureatdifferent compositions

Figure3showsthevariationofspecificheatasoffunctionoftemperatureatacompositionof30%-70%ofamixed refrigerantR290and R600a.However,astheincreaseintemperature,effect of pressure onspecificheat of a mixed refrigerantisdecreases

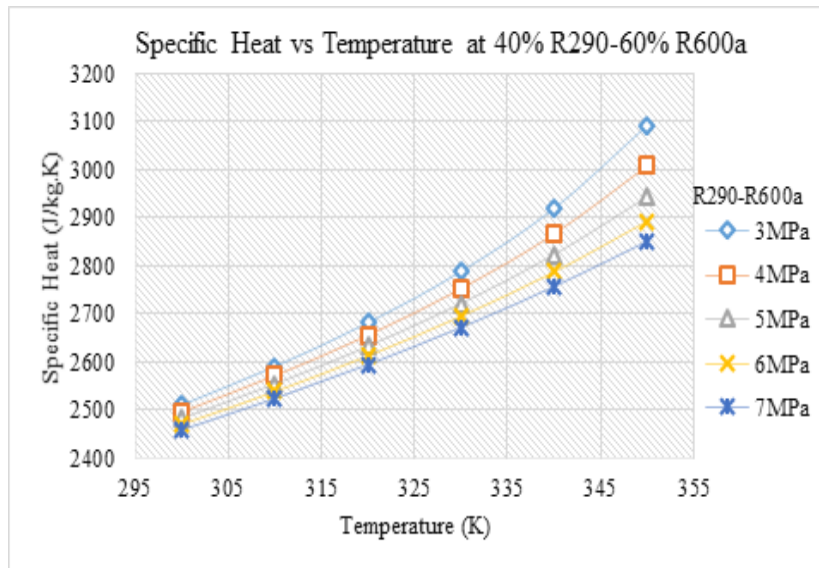


Figure4.specificheatvs.temperatureatdifferent composition

Figure4represents that variation of specific heat as a function of temperature at a composition of 40%-60% of a mixed refrigerant R290 and R600a. However, as the increase in temperature, the effect of pressure on specific heat of a mixed refrigerant decreases.

3.2. Pressure effect on thermal conductivity with respect to temperature of a refrigerant mixture at different compositions such as 10%-90%, 20%-80%, 30%-70%, and 40%-60% for propane (R290) and isobutane (R600a).

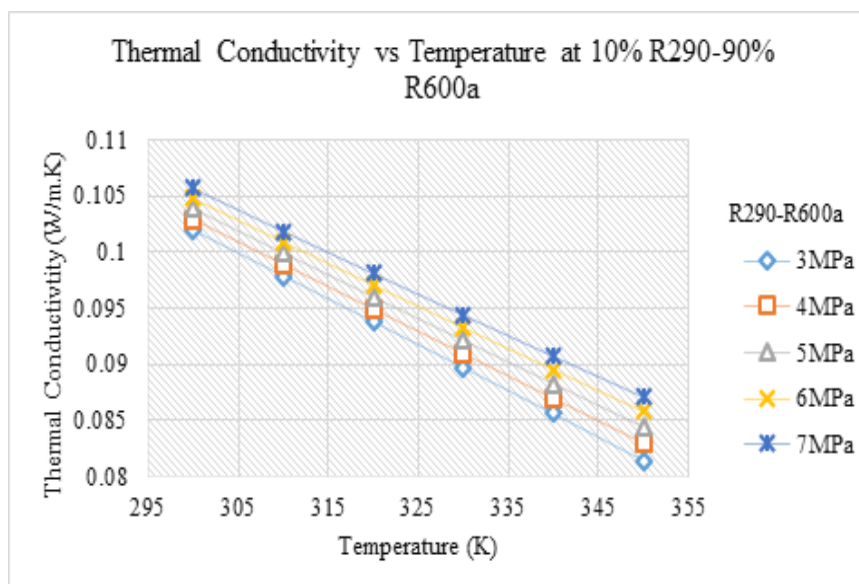


Figure5. Thermal conductivity vs. temperature at different compositions

Figure5 shows the variation of thermal conductivity with respect to temperature at a composition of 10%-90% of a mixed refrigerant R290 and R600a. Moreover, as the increase in temperature, the thermal conductivity of a mixed refrigerant also increases.

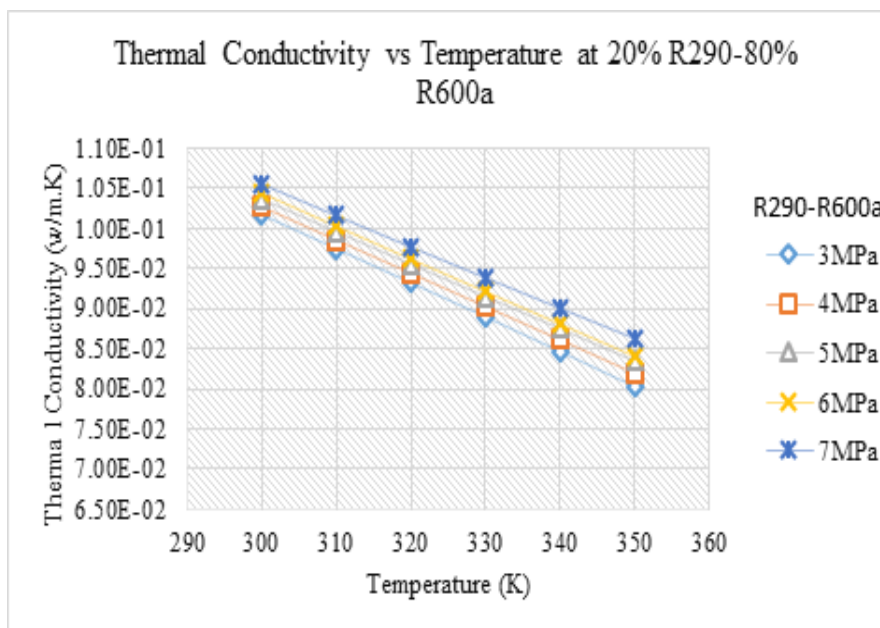


Figure6 Thermal conductivity vs. temperature at different compositions

Figure 6 shows the variation of thermal conductivity with respect to temperature at a composition of 20%-80% of a mixed refrigerant R290 and R600a. However, as the increase in temperature, the thermal conductivity of a mixed refrigerant also increases.

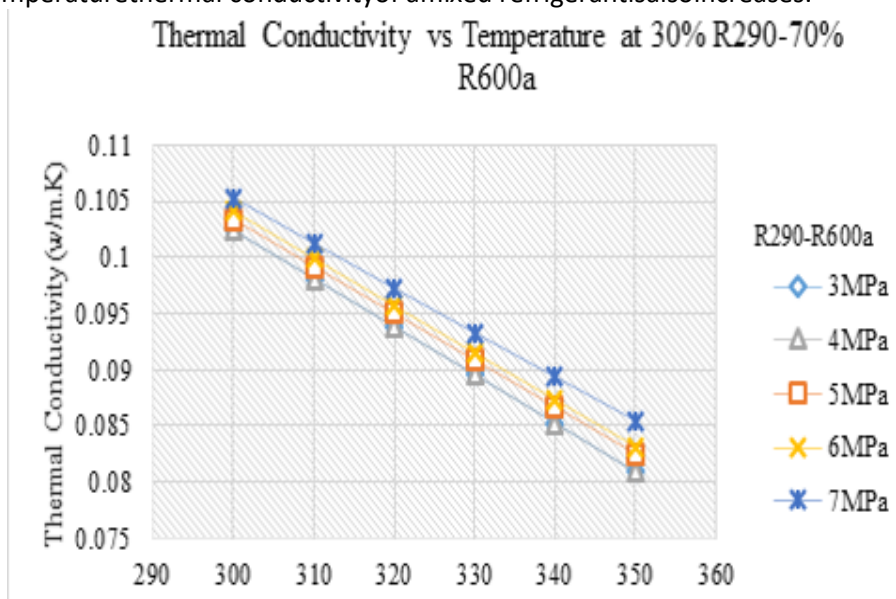


Figure 7. Thermal conductivity vs. temperature at different compositions

Figure 7 represents the variation of thermal conductivity with respect to temperature at a composition of 30%-70% of a mixed refrigerant R290 and R600a. However, as the increase in temperature, the thermal conductivity of a mixed refrigerant also increases.

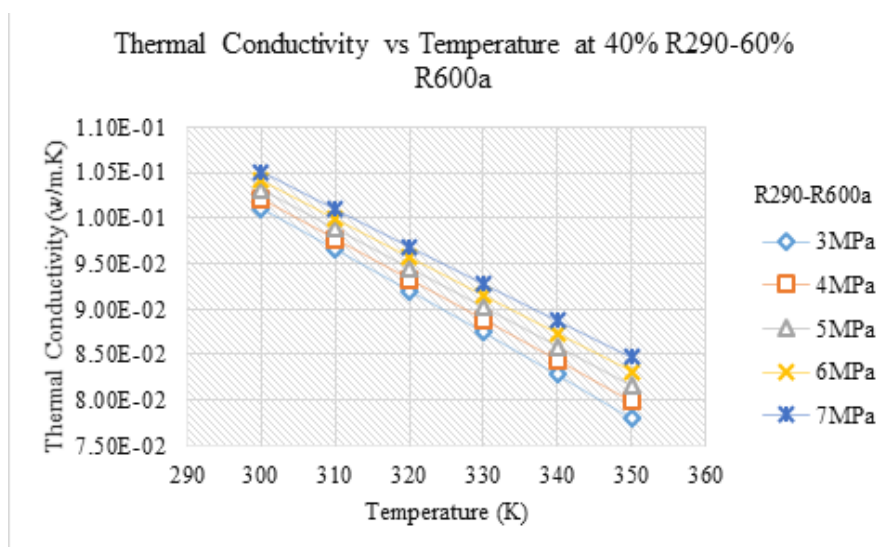


Figure 8. Thermal conductivity vs. temperature at different compositions

Figure 8 shows the variation of thermal conductivity with respect to temperature at a composition of 40%-60% of a mixed refrigerant R290 and R600a. However, as the increase in temperature, the thermal conductivity of a mixed refrigerant also increases.

4. Conclusion

In the present research work, investigation on the pressure effect of mixed refrigerants such as propane and ISO-butane are evaluated at different compositions. It was concluded that as the increase in thermal conductivity by 6.9% at constant temperature 350K. Meanwhile, the opposite trend was followed by the specific heat decrease from a temperature range of 300-350K and it reduces by 5.2% reduction at constant temperature 350K in the liquid region.

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